

# **Viscometric and Low Temperature Behavior of Lubricants with Blended VI Improvers**

**Functional Products Inc.**

**NLGI 85<sup>th</sup> Annual Meeting**

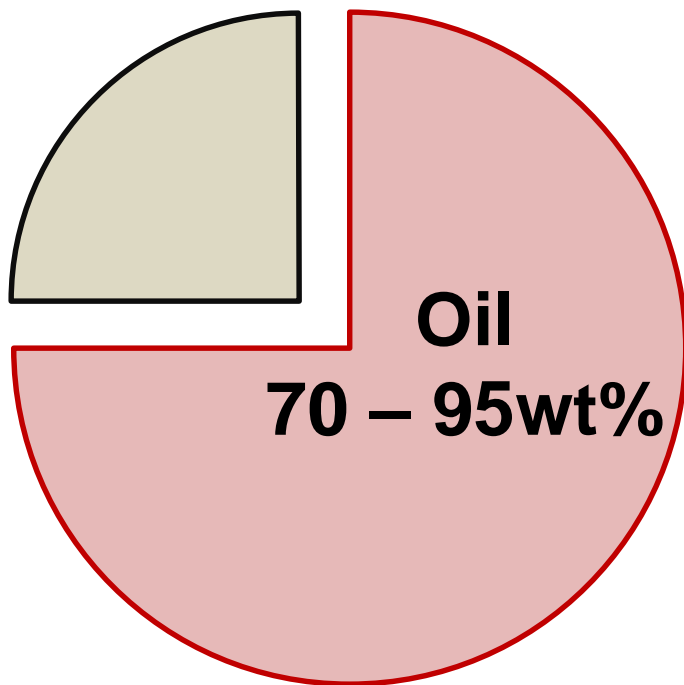
***Development Author Award Winner***



- Lubrication Fundamentals
- VII Blending Study
- Interpretation of observed trends
- Summary, future work



Thickener  
5 – 30wt%



**Gr. I/II + Naph.**

Paraffinic: VI 80-90, p.p. >-12°C

Naphthenic: VI 50, p.p. >-26°C

**Synthetics**

High VI, low p.p.

Polymeric or use thickener

**Natural / Synthetic Bio**

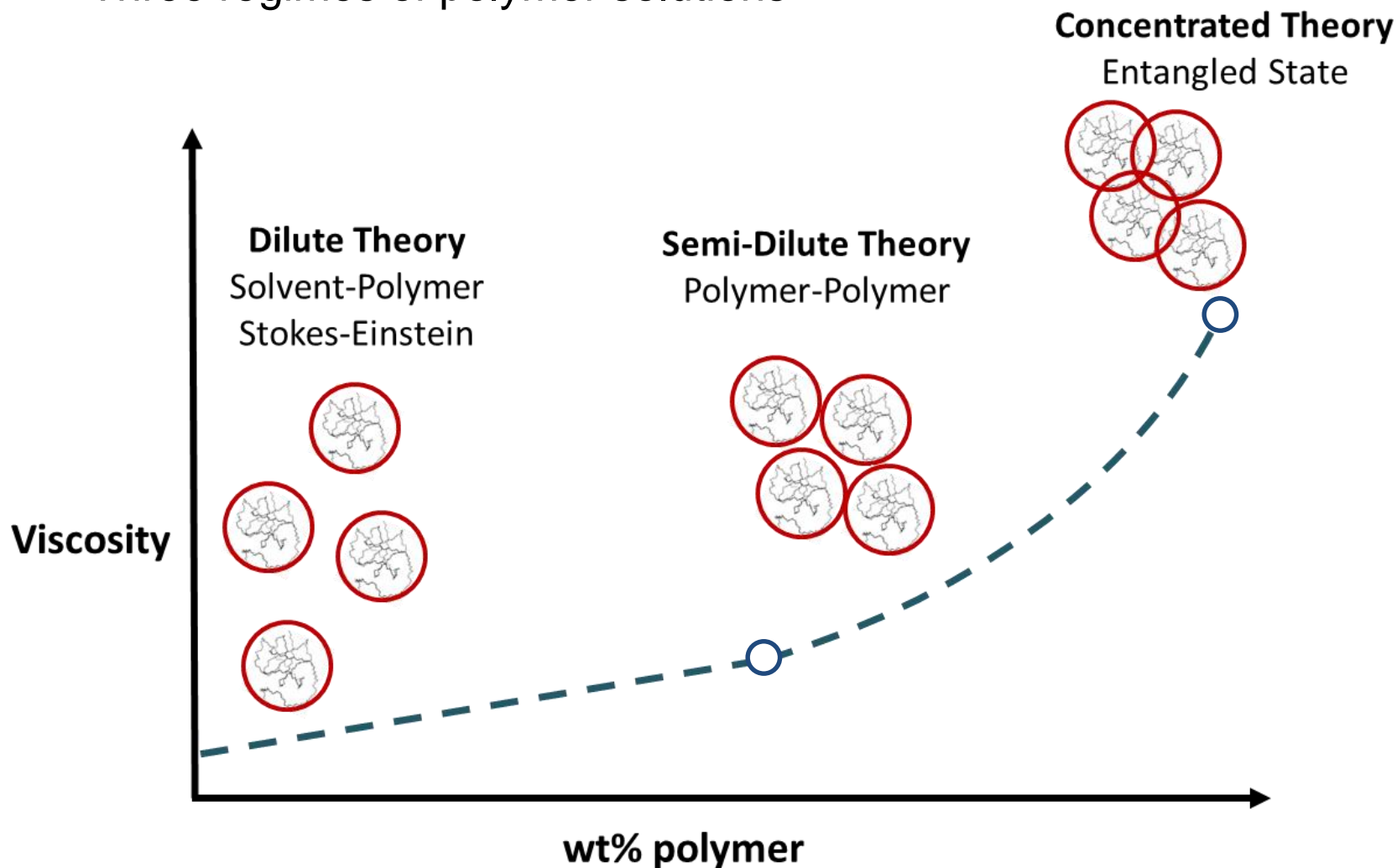
VI vs. p.p. vs. oxidation

Low viscosity requires thickener

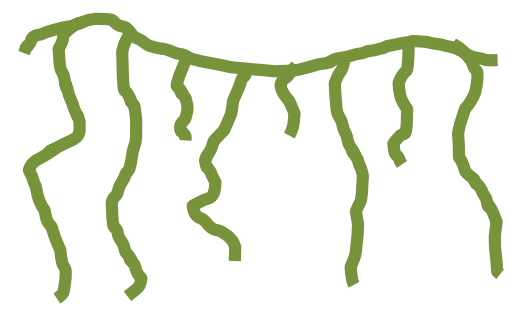


# Viscosity From Polymers

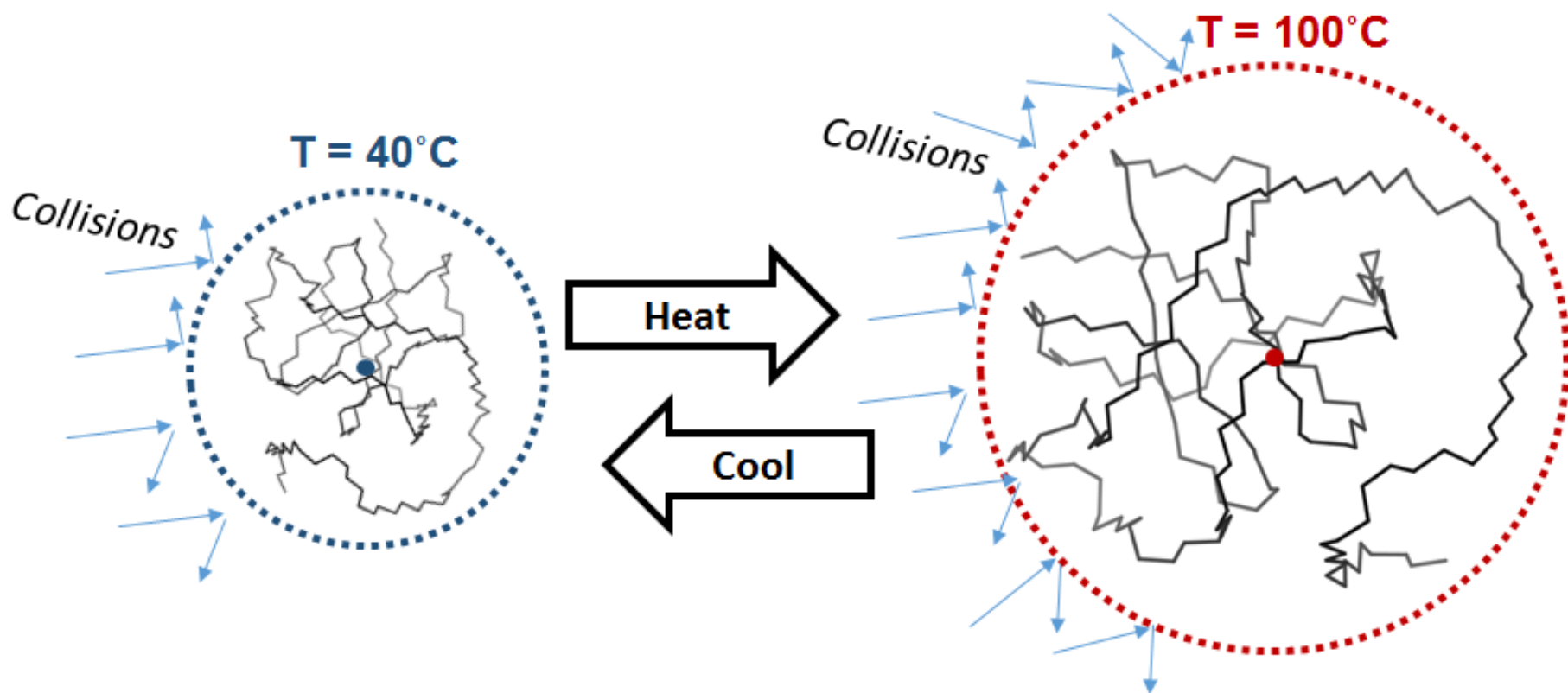
- **Polymers** are dissolved into oil to increase viscosity
  - Three regimes of polymer solutions



## ORGANIZATIONAL + CHEMICAL STRUCTURE

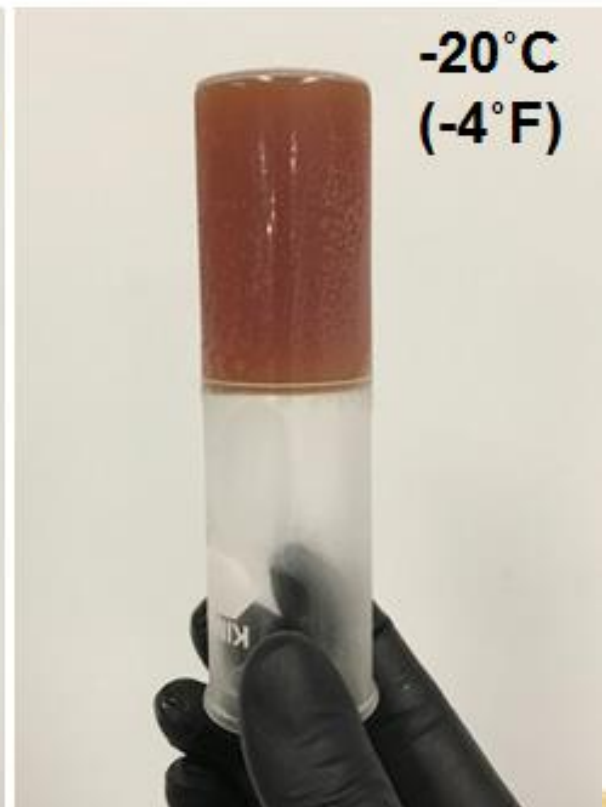
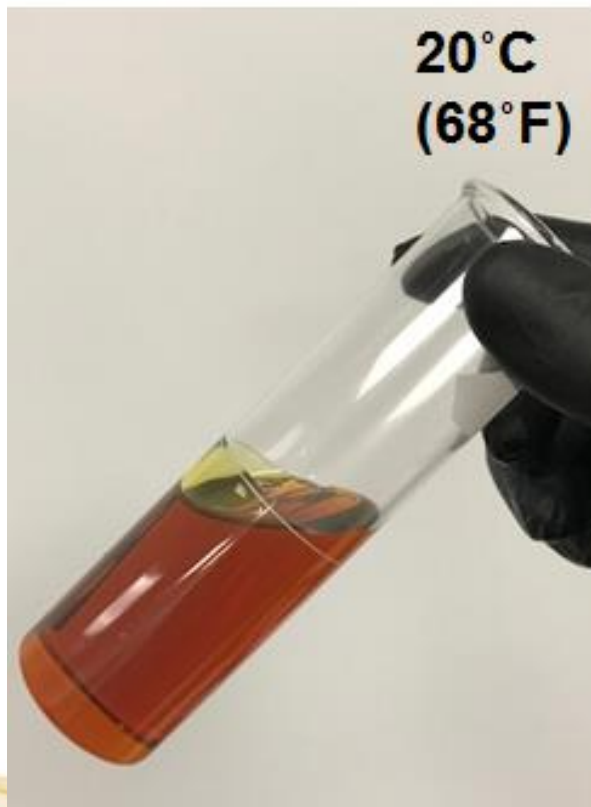


- Polymer coils dissolved in oil expand, compensate for thinning
- Ratio of KV100 to KV40, roughly (ASTM D2270)





- Temperature at which oil will not flow under its own weight
- Manual tilt test pour point (ASTM D97)



3 VI improver chemistries blended together at 5/10/20 wt%

VII	Chemistry	%Polymer wt%	MW (g/mol)	PSSI ASTM D6278	KV100 cSt	Application
“PB”	Polybutene	100%	2,000 – 3,000	0%	4000	Gear
“PMA”	Polymethacrylate	50 - 80%	10,000 – 30,000	1%	1100	Hydraulic
“OCP”	Olefin Copolymer	5 – 20%	50,000 – 100,000	22%	3500	Crankcase

Three base oils tested (0.2wt% PPD in Gr. II/III)

Oil	API	KV40	KV100	Viscosity	Pour Point, °C	Pour Point, °C
	Group	cSt	cSt	Index	No PPD	0.2wt% PPD
“Group II”	II	31.9	5	113	-18	-39
“Group III”	III	19.6	4	122	-15	-42
“PAO”	IV	30.2	6	137	-61	N/A

Blend then look at trends in VI, p.p.





- Formulations – simple premise
  - See Appendix A in technical paper for data
- Trends in VI and p.p. behavior – complex results
  - VI, p.p. varies as a function of wt% and VI improver type
  - wt% coincides with transitions in polymer solution theory
  - Why?



- 81 formulations tested using mixed VII
- Wide range of ISO/AGMA and SAE viscosity grades

Visc. Grade	#	Visc. Grade	#	Visc. Grade	#
ISO 46 / AGMA 1	2	SAE 20	2	SAE 80	5
ISO 68 / AGMA 2	8	SAE 30	13	SAE 85	11
ISO 100 / AGMA 3	7	SAE 40	13	SAE 90	12
ISO 150 / AGMA 4	2	SAE 50	12	SAE 110	13
ISO 220 / AGMA 5	6	SAE 60	4	SAE 140	10
ISO 320 / AGMA 6	6			SAE 190	9
ISO 460 / AGMA 7	2			SAE 250	2
ISO 680 / AGMA 8	0				
<b>Total:</b>	32		44		63
<b>% of Samples:</b>	40.7%		54.3%		77.8%

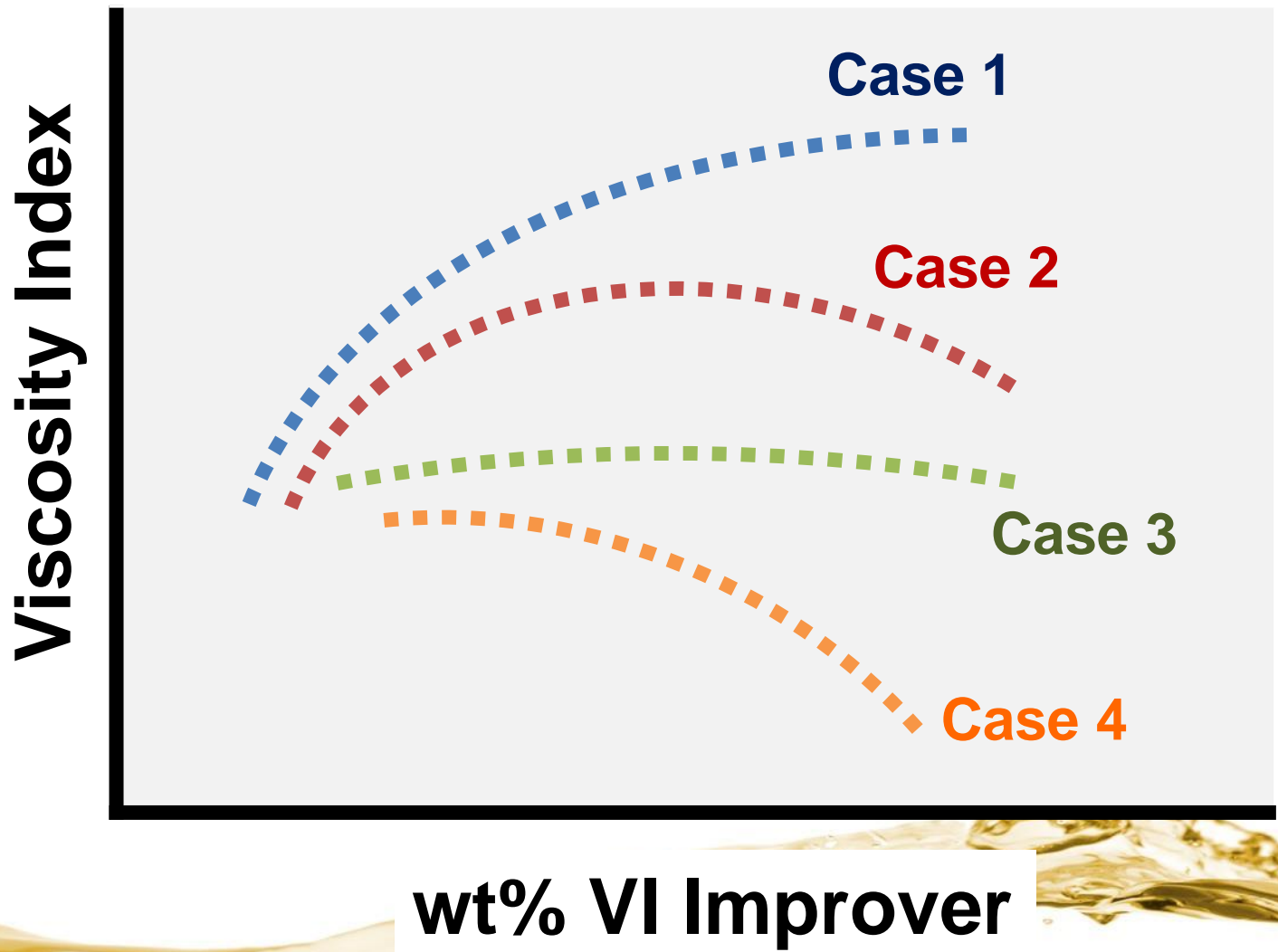


# Appendix A – By Pour Point

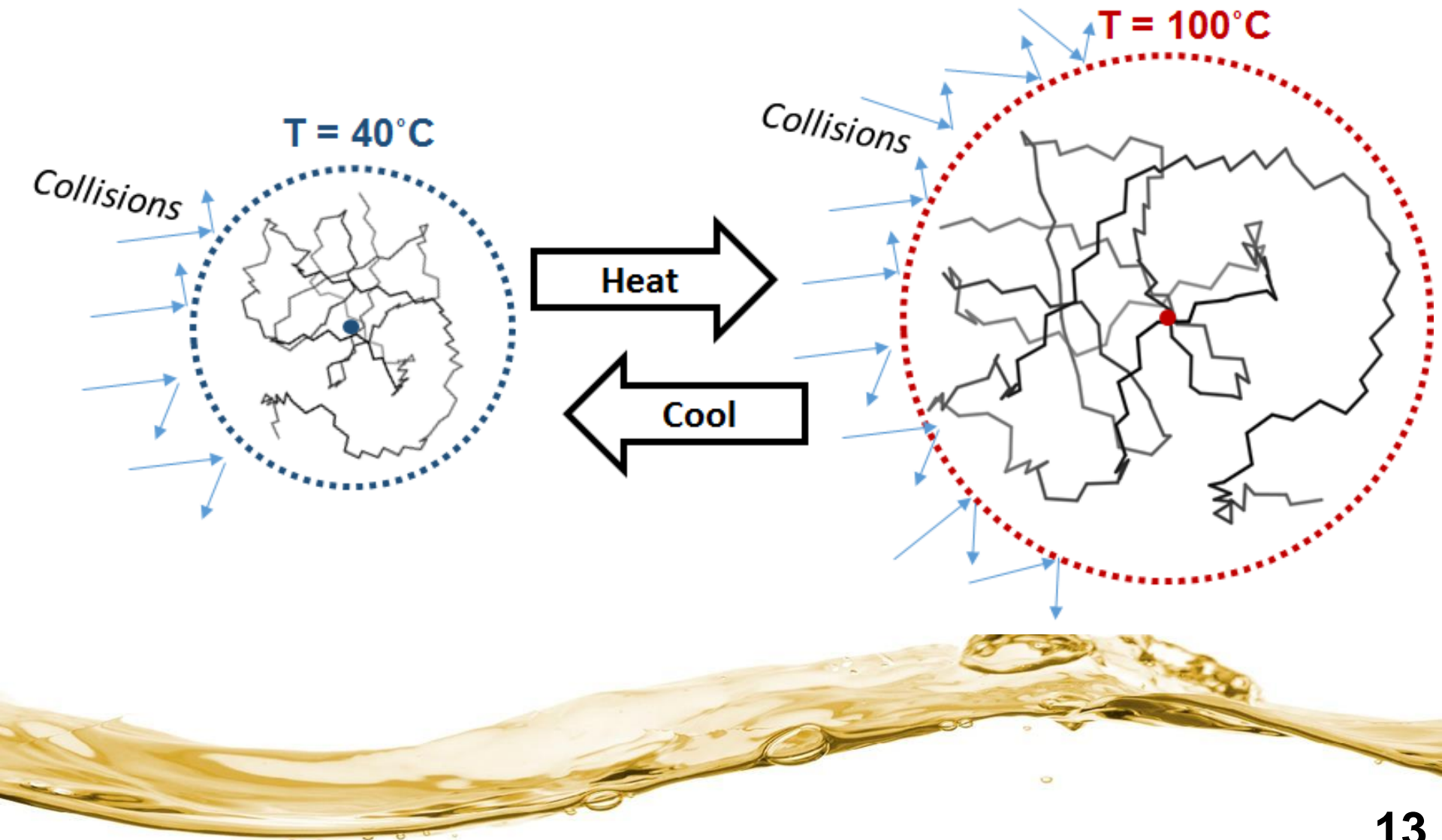


Base Oil	PPD wt%	PMA wt%	OCP wt%	KV40	KV100	VI	p.p., C	ISO VG	AGMA	SAE Eng.	SAE Gear
150N Gr. II	0.2	20	10	223.5	29.8	174	-27	220	5		140
150N Gr. II	0.2	20	5	133.7	20.2	174	-30			50	110
150N Gr. II	0.2	10	20	317.3	39.9	179	-33	320	6		190
100N Gr. III	0.2	20	5	82	15.8	206	-33			40	90
100N Gr. III	0.2	10	5	50	10.7	211	-39	46	1	30	85
100N Gr. III	0.2	10	10	80	15.4	205	-39			40	90
100N Gr. III	0.2	10	20	194.3	29.8	195	-39				140
150N Gr. II	0.2	5	5	62.8	10.6	159	-42	68	2	30	85
150N Gr. II	0.2	5	10	92.6	15	171	-42	100	3	40	90
150N Gr. II	0.2	5	20	104	16.2	168	-42	100	3	40	90
150N Gr. II	0.2	10	10	127.7	19.7	176	-42			50	110
100N Gr. III	0.2	5	5	40.6	8.3	186	-42			20	80
100N Gr. III	0.2	5	10	66.9	12.8	195	-42	68	2	40	85
100N Gr. III	0.2	5	20	182.7	28.4	195	-42				140
PAO 6		5	20	246.2	33.5	182	-44				190
150N Gr. II	0.2	10	5	66.5	11.7	173	-45	68	2	30	85
PAO 6		10	10	105.1	17.5	184	-50	100	3	50	110
PAO 6		10	5	77.1	13.3	176	-51			40	90
PAO 6		5	5	61.2	10.8	169	-52			30	85
PAO 6		5	10	91.5	15.1	174	-52	100	3	40	90

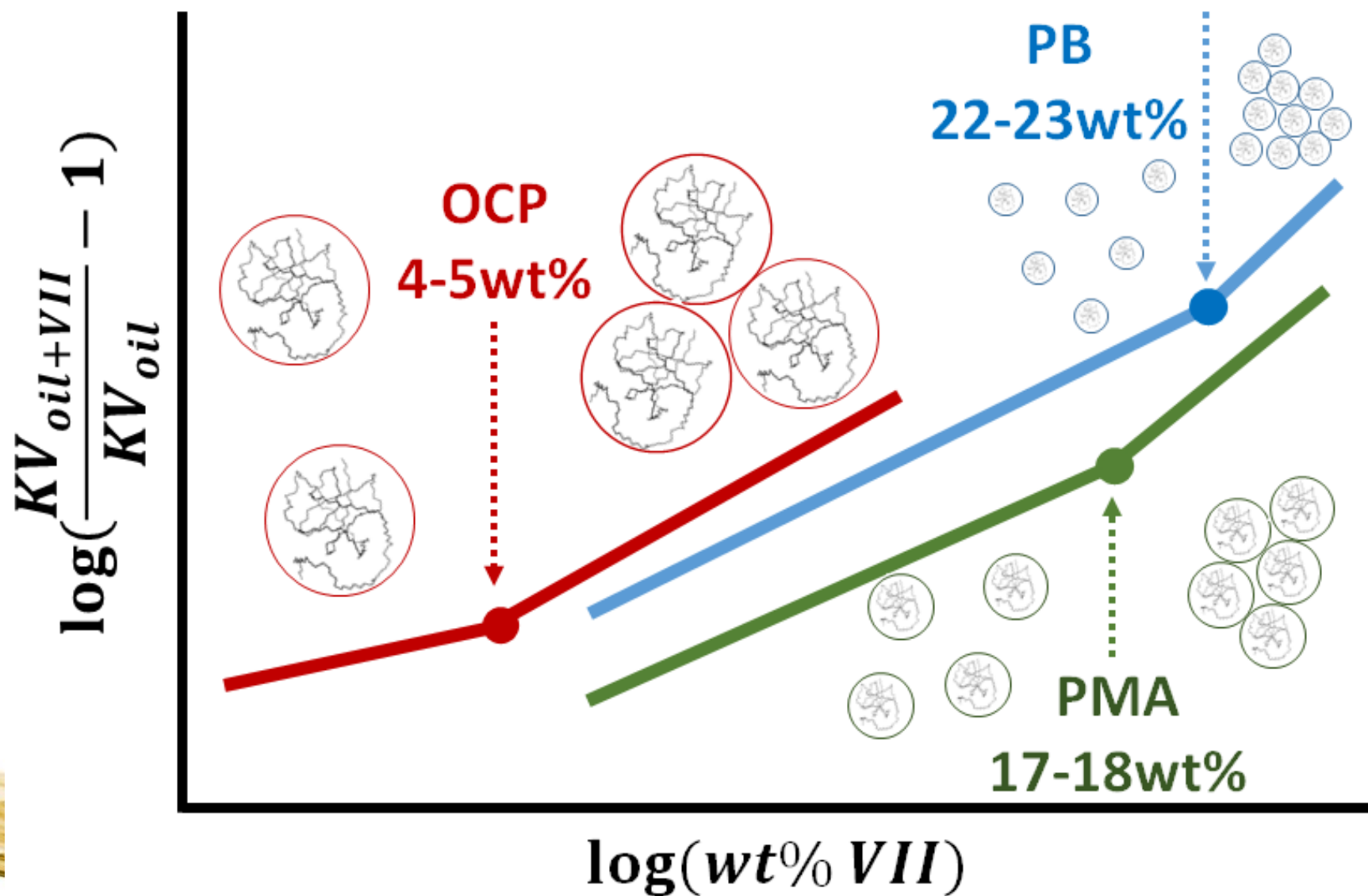




- Textbook depiction of VI improvement

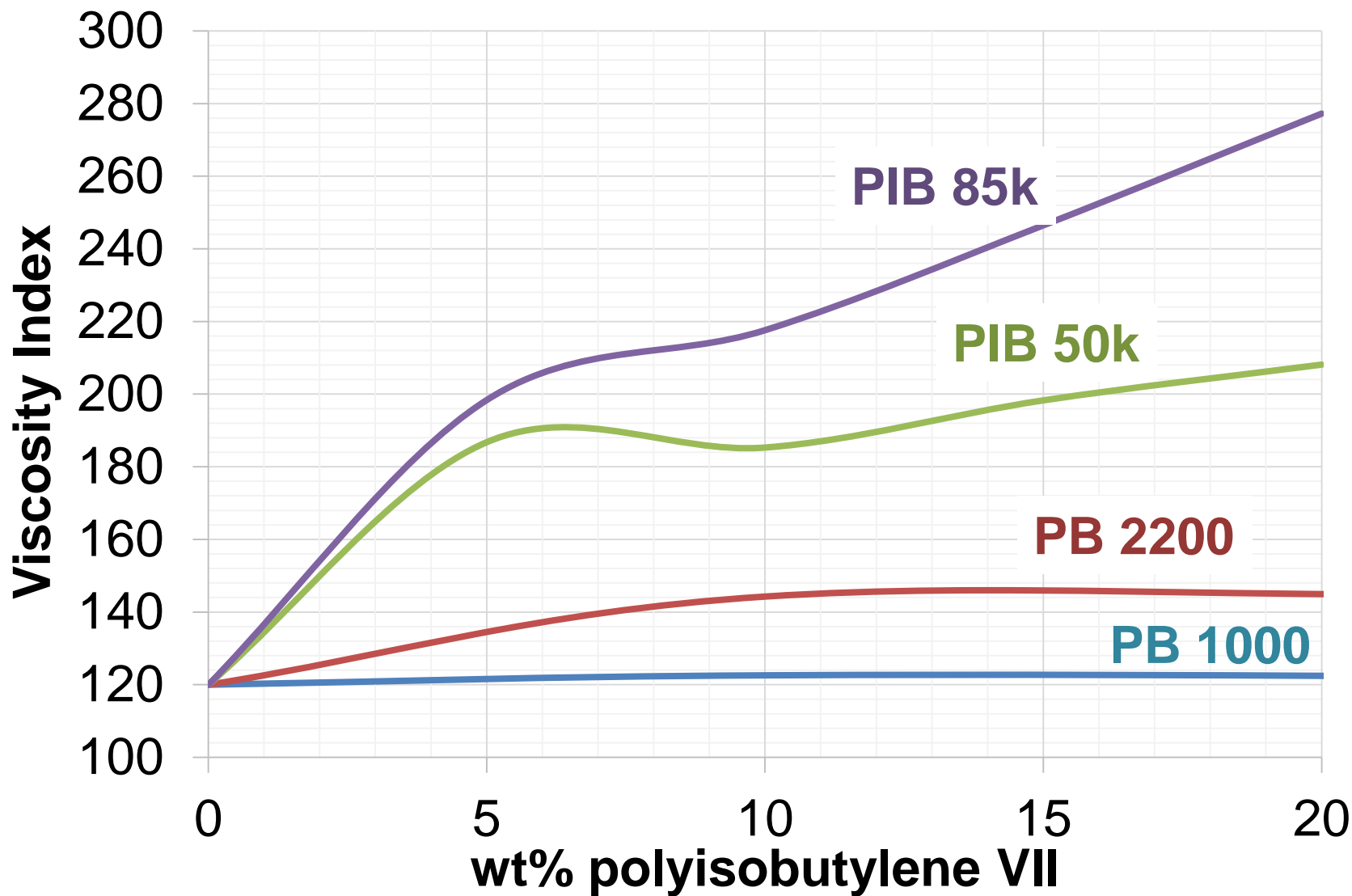


- Dilute to semi-dilute transition



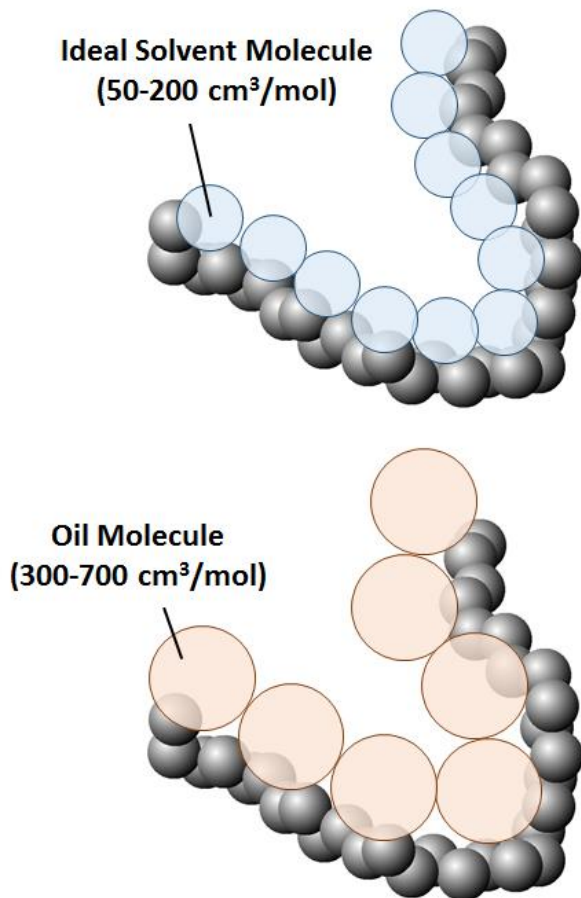


- Small polymers don't improve VI – MW drives expansion

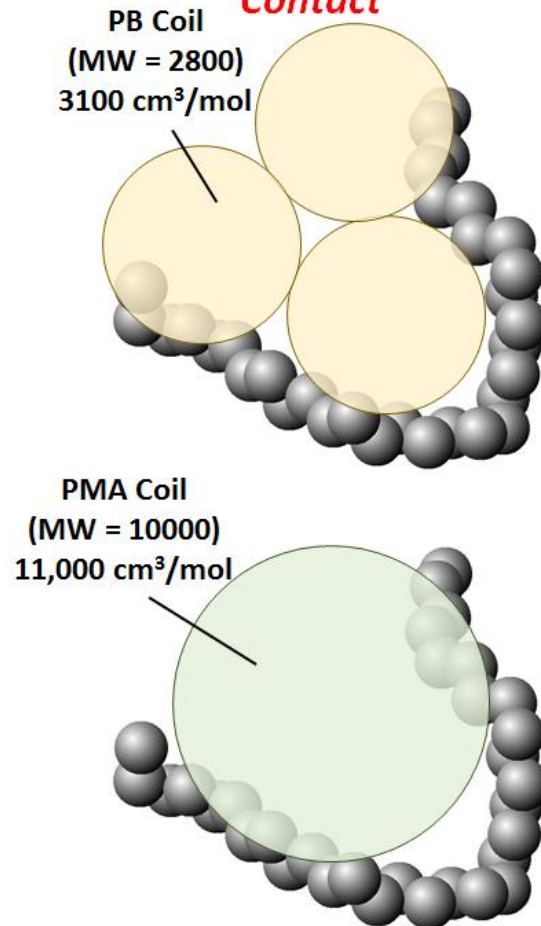


- High concentration of low MW polymer replaces solvent

### High Solvent-Polymer Contact

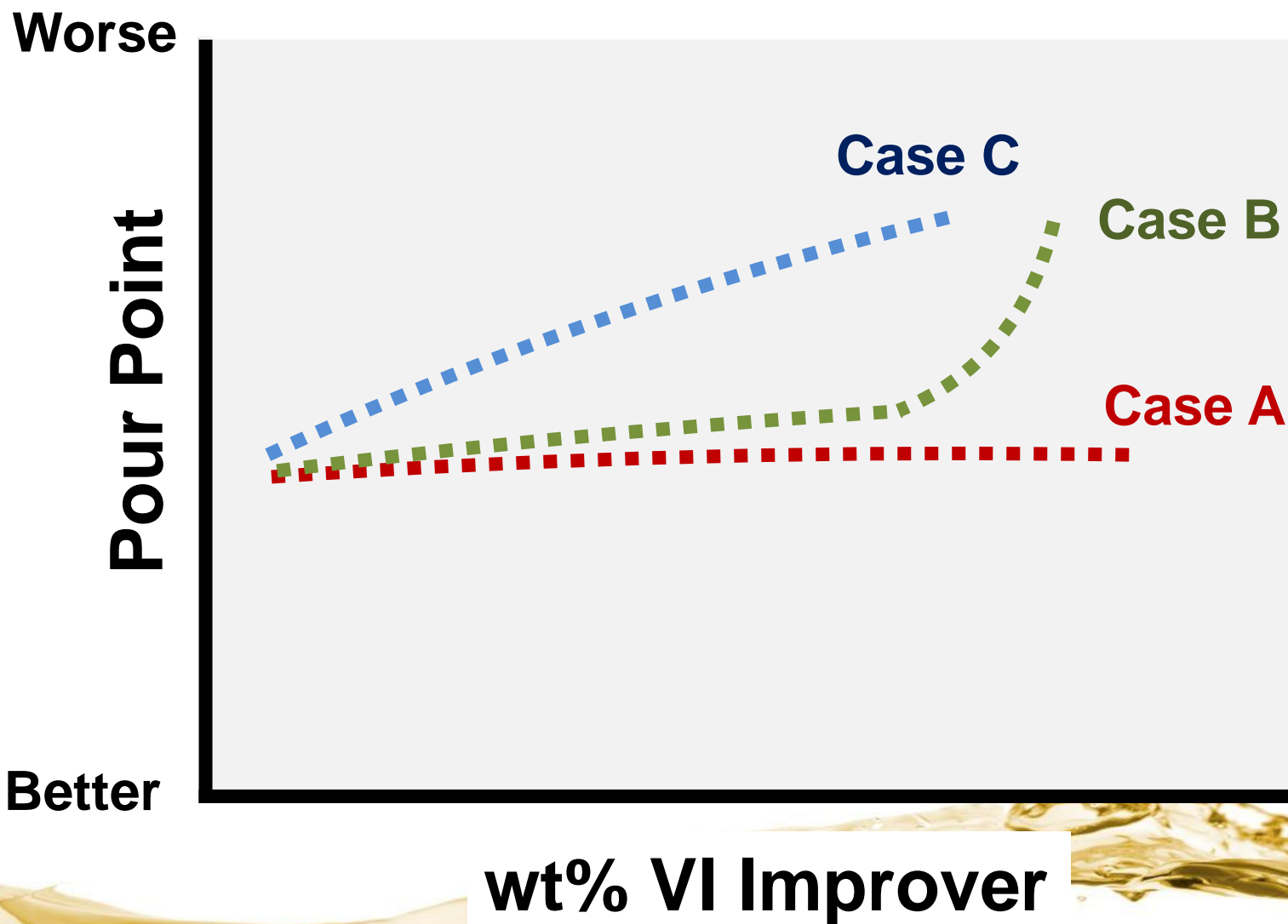


### Low Solvent-Polymer Contact



● = Monomer (50 – 100 cm<sup>3</sup>/mol)

# Findings – 3 Pour Point Trends



# Relation b/w VI and PP Cases

- Frequency table of VI trend (case 1-4) vs. p.p. trend (case A-C)
- Coincidence suggests similar mechanism

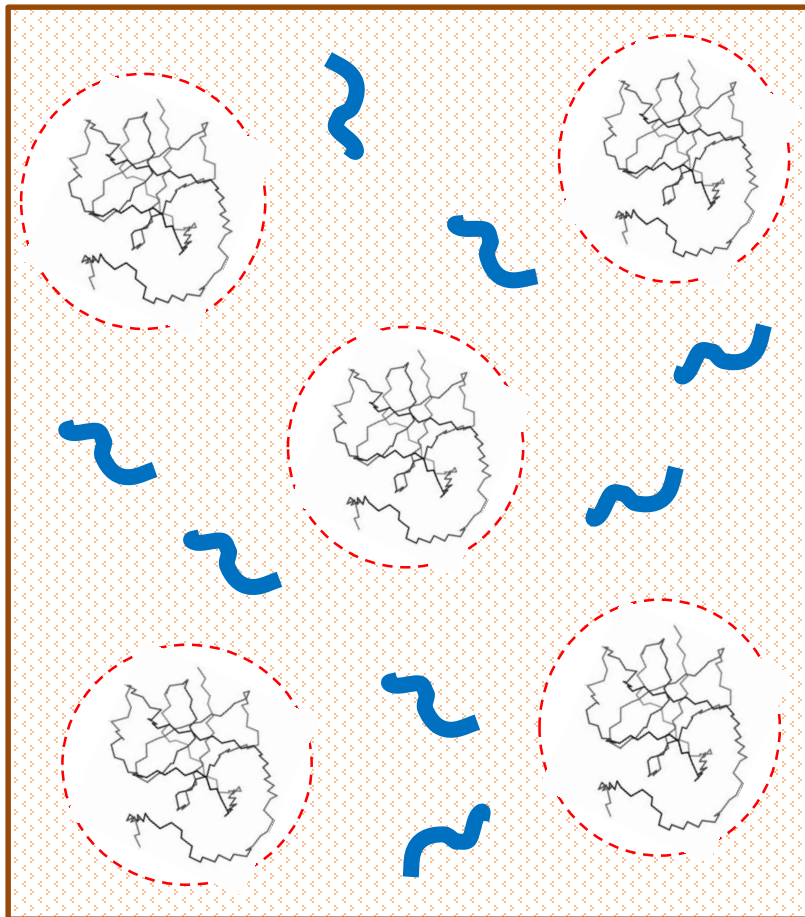
		VI Case			
		1	2	3	4
p-p. Case	A	2	4	3	<u>9</u>
	B	4	4	2	2
	C	2	<u>8</u>	1	2

Summarize what we know:

- Case 4 – decrease in VI with treat
  - Poor solubility, high KV40
- Case A – no change in p.p. with treat (ideal)
- Case 2 – VI increases then decreases with treat
  - Dilute to semi-dilute transition (coil-coil contact)
- Case C – decrease in p.p. with treat



## Dilute State

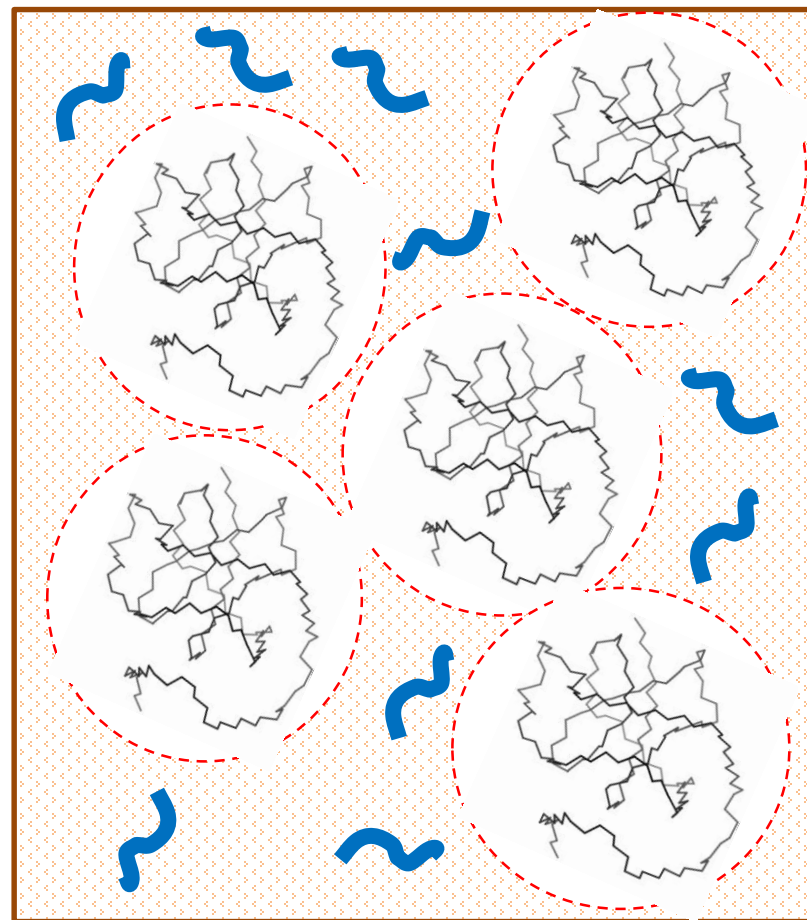


wt%  
→

Good Solv.  
→

Poor Solv.  
←

## Semi-Dilute State





- Formulations – simple premise
  - Starting point formulations for Group II / III/ PAO with VI up to 200 and p.p. to  $-52^{\circ}\text{C}$
- Trends in VI behavior – complex results
  - VI / ;p.p. trends coincide with key transitions in polymer solution theory
  - Transitions occur at wt% dependent on MW of VII
  - Further study at dilute/semi-dilute transition is needed



- Blending VII in Gr. II/III/PAO created wide data for analysis
  - Something for everyone
  - *Appendix A in technical paper*
- VI and p.p. behavior are complex
  - Simplified by grouping into qualitative trends
  - Trends explainable by fundamental principles
- ‘Semi-dilute’ condition responsible for loss of performance
  - Polymer coils in contact lose VI, worsen p.p.
  - How to avoid or mitigate this?



# Appendix A – By Pour Point



Base Oil	PPD wt%	PMA wt%	OCP wt%	KV40	KV100	VI	p.p., C	ISO VG	AGMA	SAE Eng.	SAE Gear
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# Appendix A – By Oil Group

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150N Gr. II	0.2	5	10	92.6	15	171	-42	100	3	40	90
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	<b>Trend</b>	<b>Explanation</b>	<b>Suggested Improvements</b>
<b>Case 1</b>	VI increases continuously from low to high treat	Polymer coils expand at high temperature to increase KV100; higher KV100 per KV40 means VI improves	N/A
<b>Case 2</b>	VI increases at low/medium treat; VI decreases or remains constant at high treat	Polymer coil concentration is sufficient for coil-coil interference (semi-dilute behavior)	Replace some wt% of VII with higher viscosity base oil
<b>Case 3</b>	VI unaffected by additive wt%	Polymer expansion is too small to compensate for base oil thinning at high temperature	Use higher MW VII and/or increase initial base oil VI
<b>Case 4</b>	VI decreases continuously	Polymer coils collapse due to high polymer content and/or low oil solvency	Replace some wt% of VII with higher viscosity base oil  Increase base oil solvency with low viscosity ester/AN

	<b>Trend</b>	<b>Explanation</b>	<b>Suggested Improvement</b>
<b>Case A</b>	Pour point unaffected by VII treat level	PB + OCP - Dilution of waxes by PB and polymer wt% is in dilute concentration  PB + PMA – collapse of polymer chains prevents polymer coils from accelerating wax formation	N/A
<b>Case B</b>	Pour point worsens at high treat	Similar to Case A; wax from diluent oil in VII at high treat increases total wax content of oil	Use VII with higher wt% polymer or more refined oil  Reduce VII use by increasing base oil viscosity
<b>Case C</b>	Pour point continuously worsens from low to high treat	High MW polymer coils begin to form a network in oil (semi-dilute condition) which helps the wax network form at low temperature	Reduce wt% or MW of VII to avoid semi-dilute condition  Replace some VII with high viscosity base oil